

How to Operate a Package in less-than-100% Capacity to Optimize Efficiency and Minimize Wear? Speed First.

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During the life cycle of a reciprocating compressor, conditions are likely to occur, which require running the compressor at less-than-100% capacity. For example:

- If upstream supply (i.e. suction pressure) is increased, the compressor's capacity may need to be reduced to prevent damage to the compressor and driver from overload or from operating outside permissible operating conditions.
- Reduced level of supplied gas over time may require that the compressor flow capacity be reduced in order to maintain suction pressure at a minimum acceptable level.

Different methods may be used to reduce capacity. These methods are summarized in Table 1 for an exemplary 3-stage, 4-throw unit.

	Flow, MMSCFD	RPM	BHP
Full Capacity	8.16	1500	1574
Speed	6.69	1235	1226
VVCP (68.5% Open)	6.69	1500	1303
Recycle	6.69	1500	1574
Suction Throttle	6.69	1500	1375
Single Acting	6.69	1500	1310

Frame: JGT/4

Stage 1: (2) 13-1/2ET, 13.500"

Stage 2: (1) 11-1/2ET, 11.500"

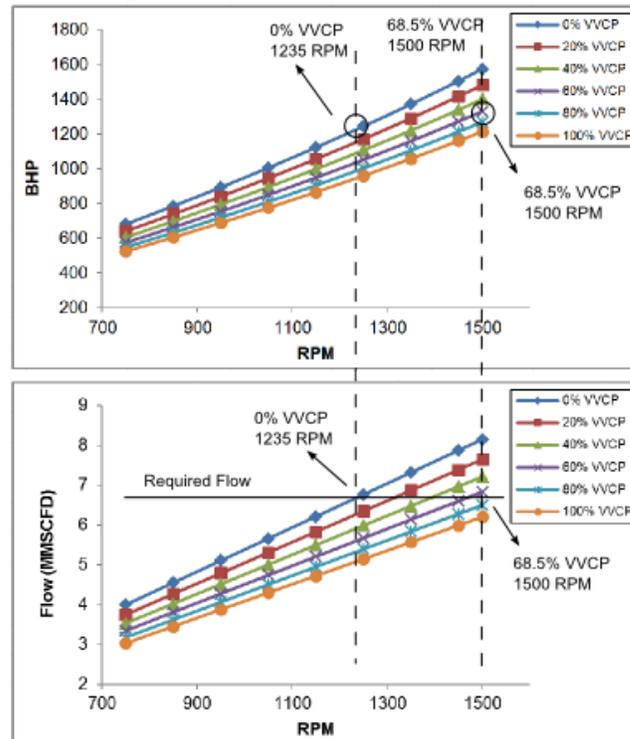
Stage 3: (1) 7-3/8ET, 7.000"

Table 1: Comparison of different methods for controlling compressor capacity

Among these methods, varying the operating speed is the first recommended method as it is an excellent way to control capacity without requiring additional equipment on the compressor. The advantages of this method are the reduced wear and tear of the machine, and increased compressor efficiency. For the configuration presented in Table 1, for example, reducing capacity by speed will reduce compressor wear and tear, i.e. RPM, by 18%. In contrast, by using a VVCP, single-acting the cylinder, or throttling, unit will unnecessarily run at full speed, whereby long-term maintenance costs are increased. Likewise, a recycle loop is very inefficient as the energy used to compress the excess gas is completely wasted and the bypassed gas also has to be cooled.

Flow versus RPM, and BHP versus RPM curves of the above 3-stage unit with the following operating conditions are shown in Fig. 1.

- Suction pressure = 40 psig
- Discharge pressure = 1000 psig
- Required Flow = 6.69 MMSCFD



Frame: JGT/4

Stage 1: (2) 13-1/2ET, 13.500"

Stage 2: (1) 11-1/2ET, 11.500"

Stage 3: (1) 7-3/8ET, 7.000"

Fig. 1: Q-RPM and BHP-RPM curves of a 3-stage compressor at operating conditions $P_s=40$ psig, $P_d=1000$ psig. Required capacity (6.69 MMSCFD) can be reached by different methods summarized in Table 1.

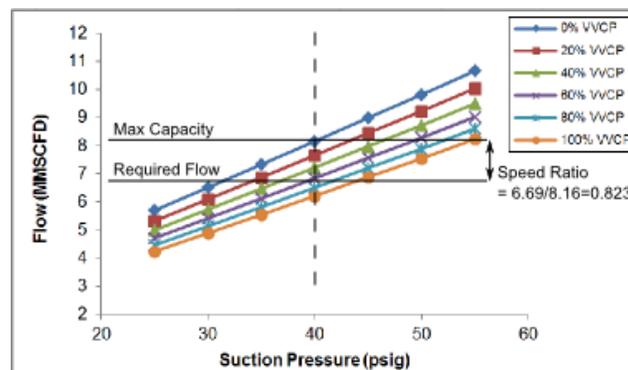
The typical procedure of selecting the optimized operating speed based on the compressor performance curve (Fig. 2) is:

1. Find performance curve with appropriate discharge pressure.
2. Find desired suction pressure and capacity point on applicable curve.
3. Ratio the desired capacity to the maximum capacity (i.e. highest performance curve) at the specific suction pressure.
4. Check to make sure the ratio multiplied by the engine speed is within the minimum operating speed of the equipment. If ratio multiplied by the engine speed is below the minimum operating speed, select the next lowest unloading step and repeat.
5. Configure the compressor for the maximum capacity unloading step and reduce the speed to the calculated RPM.

For instance, in the example of Fig. 2, maximum capacity at 1500 rpm is 8.16 MMSCFD. Therefore, the desired capacity ratio and speed are 0.823 and 1235 RPM, respectively.

$$\text{Capacity Ratio} = \text{Required Capacity} / \text{Max Capacity} = 6.69 / 8.16 = 0.823$$

$$\text{Desired Speed} = \text{Capacity Ratio} \times \text{Max Speed} = 0.823 \times 1500 \text{ RPM} = 1235 \text{ RPM}$$



Frame: JGT/4

Stage 1: (2) 13-1/2ET, 13.500"

Stage 2: (1) 11-1/2ET, 11.500"

Stage 3: (1) 7-3/8ET, 7.000"

Fig. 2: Q-Ps performance curve of a three-stage compressor at 1500 RPM, Pd=1000 psig. Required capacity (6.69 MMSCFD) can be reached by operating at 1235 RPM and 0% VVCP.

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